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Preface and Introduction

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Thank you for visiting www.EricLaine.com.

The primary purpose of this document is to serve as a memory aid for the author. Thus, the author is also the target audience. (In other words, the quality of the composition is 100% sufficient for me to understand what I wrote.)

The secondary purpose is to share this tutorial with the public. I appreciate the possibility that the general public may have some difficulty understanding the my personal abbreviations and my intuitive logic.

This presents the results of a series of single-well, radial, 3-phase, coning runs. The primary parameter is grid size.

Timestep size is also a consideration.

This is for a 720-day, black-oil simulation.

Thickness, permeability, and porosity are homogeneous by layer. Capillary pressures are modest.

The well is controlled on oil rates of 100 and 1,000 stbd.

Flowing bottom-hole pressure is limited to 3,000 psi.

The model is based on previous work by Weinstein, Chappalear and Nolan.

This study ran a 12,150-cell model in about 2 hours. The oil and the water predictions are converged. However, the gas predictions are only partially converged. Truly converged studies are not yet cost effective.

Today's computers can cost-effectively run 10,000-cell models. In contrast, studies done in the middle 1980s were run on 100-cell models. It appears that a truly converged solution requires a prohibitive number of cells, possibly 100,000.

Attempts to run a 270 x 1 x 405-cell model proved difficult. Small cells combined with the 1,000-to-100-stbd rate change at day 10 iterated excessively, even with timesteps of only 0.0001 days (8.64 seconds.)

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This presents the results of a series of single-well, radial, 3-phase, coning runs.

The primary parameter is grid size.

The five models include 10	Ox1x15	30x1x45	40x1x61	60x1x90	90x1x135
The number of cells is	150	1,350	2,440	5,400	12,150
The number of timesteps is	30	50	100	170	460
The nominal cpu seconds a	re 2	20	100	700	6000

Several factors impact run time.

Writing files to another computer and saving data for pseudo curves adds runtime.

Timestep size is also a consideration.

It is important (albeit very subjective) to converge in both space and time.

This requires advance knowledge about the converged solution.

The nominal relationship is $(dt)/(dx)^{*2}$.

Reducing the time dimension by 4 matches a space dimension reduction of 2. Timesteps typically need to be smaller whenever there is a rate change.

There is a balance between how small, convergence tolerance, & cell size. This study also considers the effect of the maximum timestep size.

This study used a SUN ULTRASPARCII workstation running at 440 Mhz with 256Mb of RAM and 2 Mb of L2 cache. SUN currently offers cpu speeds up to 600 Mhz.

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This report discusses saturation maps and production plots from the simulations. There is some discussion about calculating well indices (for the perforated cells.)

The oil-saturation maps are for vertical cross sections. The cross sections show the water and gas coning through time. The wellbore is on the left.

The production plots are grouped for easy comparison: Production ratios and flowing-bottom-hole pressures, Production rates and a close-up view of flowing-bottom-hole pressures, and Production cumulatives and average reservoir pressure.

A spreadsheet highlights the input variables for calculating the completion factors.

A summary of the simulated results for the $30 \times 1 \times 45$ case is in the appendix.

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ω đ, 29 Each of the RZ cross sections is an oil-saturation map. There are two versions of the 10 x 1 x 15 cross section (an overview and a close up,) and there are close-up cross sections of the 30 x 1 x 45 model.

The overview 150 cells from 0.25 to 2050 ft. This pictures the important features of the reservoir:

Perforation locations.

Transition zones:

Gas-oil capillary pressure, and

Oil-water capillary pressure.

However, there is too little detail to show the coning.

The close ups (of the $10 \times 1 \times 15$ model) enlarge the cells closest to the perforations. The perforated cells and the transition zones provide reference points. The water cone and the gas cone are easy to see.

The close ups (of the 30 x 1 x 45 model) also zoom into the near-wellbore cells. This is the same area covered by the second cross section. The additional detail gives better views of the water and the gas cones.

The plots consistently support the conclusions drawn from the cross sections.

There has been considerable discussion about which fluid phase wets reservoir rock. The reality is that any phase might be the dominate wetting phase. It is also possible for two phases to share wetness.

The capillary pressures used for this study are for: A water-wet aquifer, A water-wet oil zone, and An oil-wet gas cap.

A phase (water, oil, or gas) can only flow at saturations above the critical saturation. This also means the phase relative permeability is above zero.

The gas-oil and the water-oil contact depths are defined as follows. Gas saturation is at (or below) the critical gas saturation below the goc. Oil saturation is at (or below) the critical oil saturation below the woc.

Interfacial-surface tension forces wetting phases beyond the contact. In this study: Mobile oil rises above the goc, and Mobile water rises above the woc.

Note: negative capillary pressures indicate an oil-wet aquifer and a gas-wet oil zone. Mobile gas would exist below the goc, and

Oil saturation is at (or below) the critical oil saturation above the goc. Mobile oil would exist below the woc.

Water saturation is at (or below) the critical water saturation above the woc.

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		Water C	one		
The first close up shows	that water	cones (up te	o the lo	ower per	foration) within 10 days.
The second and third clo Controlling (healing	ese ups sho) the cone a	w that the c at this rate i	ones a s proba	are stable ably une	e (no change) at 100 stbd. conomic.
The rest of the close ups	show the	water cone	growin	g.	
		Gas Co	ne		
The gas may have reach The probability of ga	ied the upp as breakthr	er perforatio ough is eve	on as e n high	early as c er by day	day 100. y 200.
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သံ 오 29 **Discussion**, Saturation Maps

Both grid sizes show the same gas-coning trends.

However, the gas cone is closer to the upper perforation by 100. Perhaps the finer grid is predicting more coning: Gas breakthrough might be sooner, or More gas may be breaking through. This appears to be a convergence issue.

In summary, grid size affects the gas coning predictions. The sizes of the water cone and the gas cone increase with time. It appears uneconomical to control coning with a lower oil rate. Finer grids should be investigated (for convergence.)



Each group of plots provides an easy comparison of related data. Production ratios and flowing-bottom-hole pressures, Production rates and a close-up view of flowing-bottom-hole pressures, and Production cumulatives and average reservoir pressure.

All three groups look at solution convergence as a function of grid resolution. The first set of plots tends to be the most useful, especially for history matching.

Oil rate is a common input, either for history matching or as a production target. Naturally, gas rate would be input for a gas field.

It is easier to compare ratios (water cut and produced gas-oil ratio) than rates. This is equally true for history matching and for comparing field-development scenarios.

It is also easier to compare ratios than cumulative production. The summations give larger values that automatically mask rate variations. Integration smoothes data whereas. Differentiation introduces noise.

This study focuses on the effect of grid size on coning performance.

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All the grids switch to bottom-hole pressure control near 300 days. The ratio plots clearly indicate the 10 x 1 x 15 grid is unconverged. This grid is too coarse. The finer grids give converged values. The exception is the produced gas-oil ratio. Increasing grid resolution shows a trend towards convergence. The produced gas-oil ratio diverges: at about 60 days for the 10 x 1 x 15 grid, at about 120 days for the 30 x 1 x 45 grid, at about 180 days for the 40 x 1 x 61 grid, and at about 200 days for the 60 x 1 x 90 grid. This suggests that a much finer grid will be needed to get a converged gas-oil ratio. Perhaps a 120 x 1 x 180 or a 180 x 1 x 270 grid will converge. These will be much longer runs. A 21,600 cell run might be six to ten hours. An 86,400 cell run might be 18 to 40 hours. Neither run was considered cost-effective for this study. Engineering judgement suggests treating gas-oil ratio convergence as a sensitivity item. The divergence time is approaching the asymptotic portion of the curve. Perhaps the limiting gas-oil ratio is near 4.2 Mscf/stb.



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The next set of plots includes a close up of the flowing-bottom-hole pressure. Pressure control replaces oil-rate control at about the same time for all grids. The switch seems to happen between 275 and 290 days.

This is a narrow range.

The exaggerated scale of the close-up plot is visually misleading.

The rate plots, like the (previous) ratio plots indicates: The 150-cell grid is too coarse to converge, The finer grids all converge for flowing-bottom-hole pressure, The finer grids all converge for water production, however, Gas production is (probably) not yet converged.

The gas-rate divergence times are about the same as for the gas-oil ratio.

The predicted gas rate seems to: Be a little later as grid resolution (fineness) increases, Peak a little higher as fineness goes up.

In addition, the decline ratio looks like it is about the same for all grid resolutions.

Engineering judgement suggests treating gas-rate convergence as a sensitivity item. The divergence time is approaching the switch to pressure control. Perhaps the limiting gas rate is just below 4,000 Mscfd.

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The cumulative plots tend to support previous (ratio and rate) conclusions.

The cumulative-produced-gas plot disguises the divergence times because it takes awhile for the (relatively) small rate differences to add up to noticeable cumulative differences.

Most of the cumulative difference happens at the end of the second year.

Engineering judgement suggests treating cumulative-gas as a sensitivity item. Perhaps the limiting gas quantity is about 100 MMscf higher at 720 days.



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Discussion, Production Plots

Convergence is clearly a function of grid resolution. None of the grids fully converged for gas production.

This casts doubt on using a 10 x 1 x 15 grid for the Second SPE Comparative Study Project. A review of JPT, March 1986, pp345-53 is in order.

Grid resolution is a relative term. Contemporary computers now run two orders of magnitude faster. This indicates that a $10 \times 1 \times 15$ was a fine-grid model in 1986.

In summary, the 60 x 1 x 90 grid resolution (with its 15-minute run time) is great predictor for water coning (with today's computers.) The same grid is an adequate predictor for gas coning, provided the economic analyses reflect the sensitivity to gas coning.

Faster computers will continue to redefine the fine and coarse adjectives used to characterize relative cell sizes.

Convergence is clearly a function of grid resolution. The finer grids converge nicely for water production. They also converge well for flowing-bottom-hole pressure. None of the grids fully converged for gas production. This study concluded converged runs would NOT be cost effective. Engineering judgement extrapolated the gas values. The increasing gas coning does seem reasonable. Gas preferentially cones into the cell closest to the top perforation. This becomes more noticeable as the cell sizes get smaller. The gas saturation is higher with finer grids. Gas relative permeability is also higher with finer grids. This means gas cones faster with finer grids (which is what the models tell us.) Alas, there is no convergence. The obvious mathematical recommendation is to further reduce the cell size and the timestep size. The equally obvious engineering solution is to recognize the trade-off between study cost and field profitability. An extra 100 MMscf production (7%) in the second year has a small impact. Sales increase about \$200,000 (at \$2 / Mscf.) This adds to the oil and the other gas sales. Other gas sales are \$3,000,000 (for 1,500,000 Mscf.) Oil sales are about \$11,000,000 (for 550,000 stb at \$20 /stb.) The net effect is a 2% increase in gross revenue. Intuitively, marginal projects become unattractive with a 2% revenue reduction.

The next group of plots focuses on the gas plots (ratio, rate, and cumulative.) The solid line is from the previous plots for: The 90 x 1 x 135 grid, and A maximum timestep of 44 days. The symbols are from a special model with: A 90 x 1 x 135 grid, and A maximum timestep of 0.5 days. The results appear to be identical. The largest difference for the production and pressure variables is 1.6%. Only four differences are greater than 1%. The results are identical (within engineering accuracy.) In addition: The runtimes were within 5%. The runtimes were within six cpu minutes (out of two hours.) Curiously, the faster run was for the 0.5-day maximum timestep. This may not be a general result. In general, there is some timestep size that optimizes the iterations.



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Gas Plots and Timestep size



Completion Factors (Well Indices)

Calculating completion factors (well indices) is straight forward. The calculation must be completed for each completed cell (grid block.) It is easy to overlook a variable.

The simulated results are rather insensitive to completion factors. This does NOT justify introducing careless errors.

Completion factors are the time-invariant portion of productivity indices.

Peaceman developed a robust procedure for calculating completion factors. Peaceman's procedure works for vertical and horizontal wells. Eclipse uses Peaceman's procedure.

There is a difference between grid-block and field productivity. Simulators must use grid-block productivity. Grid-block productivity accounts for the well-to-cell connection.

Please note that many authors have derived productivity-index equations. Some of these equations give productivities that differ by an order of magnitude. One cause seems to be grid-block versus field productivities.

Completion Factor Spreadsheet

See J_ect.ppt for backgro ECLIPSE's connection factor = ECLIPSE's connection factor = Ereld (m ³ cp) 0.001127 Metric (m ³ cp) 0.001127 = conversion constant (0.0011) (m ³ cp) 6.283185 = sector angle, radians (cm ³ cp) 6.283185 = sector angle, radians (cm ³ cp) 6.283185 = sector angle, radians (cm ³ cp) 6.1333 = first perpendicular-to-wellbory (cm ³ cp) 6.13333 = net thickness, ft (m or cm) (cernent o.dl) 1.3333 = net thickness, ft (m or cm) (cernent o.dl) 1.3333 = ret (m or cm) (field outer radians) (dl) 0.25 = rw, ft (m or cm) (field outer radians) (dl) 1.16206449 = ret ft (m or cm) (field outer radians) (dl) 0.29051612 = lst cell outer radius, ft (dl) 1.183941 = RADIAL-VELL perforation (dl)	ound informatio = (J)'(Bo)'(Muo)/(K)/(day'bar) p)/(day'bar) cp)/(hr'atm) cp)/(hr'a	n. (ro) 08527 for metric, 1 md or md) r md) r md)	input = solid, bold, red box & numbers intermediate = black letters only output = bold, dashed, blue box & numbers instructions = bold, purple letters 0000 ????????????? for lab) 0000 ?????????????????????????????????
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The 60 x 1 x 90 grid resolution is appropriate for this coning study. Adding cells improves convergence and increases runtime.

The common adjectives for describing grid resolution (fine and coarse) are relative terms that reflect cost-effective engineering (with "today's" computers.)

The $10 \times 1 \times 15$ grid resolution was a fine grid in the mid 1980s. The mid 1980s grid may not have been a converged solution, yet It was a cost-effective solution.

Today a 60 x 1 x 90 grid is considered "fine" resolution. It is only converged for pressure and water, although It is NOT converged for gas, yet It is cost effective.

Tomorrow's computers will use a 270 x 1 x 405 grid for fine-scale studies. It seems likely that this will be a fully converged solution, including gas.

Several factors impact run time.

Runtimes increase about 33% when files are written to another computer. Runtimes increase about 33% when pseudo-curve files are saved.

Timestep size is also a consideration.

Maximum timesteps of 0.5 and 44 days are compared. The results are identical (for practical use.)

Use a spreadsheet to calculate the completion factors (It helps avoid errors.)

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þ	0.42368	0.42927	0.43781	0.44429	0.43517	0.42925	0.42328	0.39542	0.36692	0.34956	0.33012	0.31655	0.30178	0.27194	0.26200	0.25123	0.21844	0.20122	0.18416	0.16582	0.15365	0.14506	0.12400	0.11620	0.12590	0.12717	0.12950	0.12932	0.1019	0.11354	0.11148	0.11051	0.11105	0.11422 0.11740	0.11620	0.11797	0.11927	0.12003	0.12023	0.12021	0.11407	0 44 407			FWU	T/W/T
-	1.33146	1.33140	1.33137	1.33287	1.44913	2.33471	3.47304	3.40310	3.30866	3.24429	3.16601	3.09584	2.99969	כחכר / יק	2.58550	2.42306	1.96822	1.75734	1.57219	1.43411	1.38773	1.38172	1 38301	1.38431	1.38505	1.38493	1.38442	1.38288	1 37688	1.38297	1.38108	1.37921	1.37676	1.37397	1.36684	1.36302	1.35929	1.35584	1.35294	1.34941	1.34169			msclystp	WGOR	500
	3345.23	3344.98	3344.27	3343.48	3345.25	3341.78	3000	3000	3000	3000	3000	3000	3000		3022.21	3046.00	3115.45	3149.16	3181.38	3215.95	3238.89	3254.60	3250.10	33U3.U4	3590.00	3590.43	3590.75	3591.15	3591 44	3313.04	3318.88	3324.46	3328.04	3330 44	3335./J	3339.91	3345.80	3353.40	3362.61	3372.81	3790 78 142#.4	3028.22		psia	VUBHT	10000
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Appendix - 30 x 1 x 45 Simulation Results Table

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